

# Supporting Information

**Control of exposed crystal planes of CeO<sub>2</sub> enhances electrocatalytic nitrate reduction**

**Fei Wang<sup>1,2,#</sup>, Dan Li<sup>1,#</sup>, Jian Mao<sup>1</sup>**

<sup>1</sup>College of Materials Science and Engineering, Sichuan University, Chengdu 610065, Sichuan, China.

<sup>2</sup>Faculty of Materials Science and Engineering, Kunming University of Science and Technology, Kunming 650093, Yunnan, China.

<sup>#</sup>Authors contributed equally to this work.

**Correspondence to:** Prof. Jian Mao, College of Materials Science and Engineering, Sichuan University, No.24 South Section 1, Yihuan Road, Chengdu 610065, Sichuan, China. E-mail: [maojian@scu.edu.cn](mailto:maojian@scu.edu.cn); Prof. Fei Wang, Faculty of Materials Science and Engineering, Kunming University of Science and Technology, No. 727 Jingming South Road, Chengong District, Kunming 650093, Yunnan, China. E-mail: [echo1994wf@foxmail.com](mailto:echo1994wf@foxmail.com)

## 1. Determination of ammonia-N

The determination of ammonia-N was performed using a modified indophenol blue spectrophotometry method.<sup>1</sup> Initially, a specific volume of electrolyte solution was extracted from the cathodic electrolytic cell and diluted to 2 mL. Subsequently, 2 mL of a 1 M NaOH solution containing 5 wt% salicylic acid and 5 wt% sodium citrate was added to the diluted solution. Additionally, 50  $\mu$ L of a 5.5 wt% NaClO solution and 0.2 mL of a 1.0 wt%  $C_5FeN_6Na_2O$  solution were introduced. The mixture was thoroughly shaken and allowed to stand at room temperature for 2 hours to undergo the necessary reactions. Following the reaction period, the absorption spectrum of the resulting mixture was measured using a UV-visible spectrophotometer within the wavelength range of 550-750 nm. The concentration of ammonia-N was determined by analyzing the absorbance at 655 nm. To establish the calibration curve, a series of standard  $NH_4Cl$  solutions (0, 0.25, 0.5, 1.0, 1.5 and 2 mg  $L^{-1}$ ) were prepared ( $NH_4Cl$  crystals were pre-dried at 105  $^{\circ}C$  for 2 hours to ensure the accuracy of the standard solutions), By plotting the concentration of the  $NH_4Cl$  solutions against their corresponding absorbance values at 655 nm, a calibration curve was generated. This curve could then be used to determine the concentration of ammonia-N in the tested samples based on their absorbance readings at 655 nm.

The ammonia yield rate was calculated by the Equation 1:<sup>2</sup>

$$\text{Yield}_{NH_3} = (c_{NH_4^+} \times V) / (M_{NH_4^+} \times t \times m) \quad (1)$$

The FE of NRA was calculated by the Equation 2:

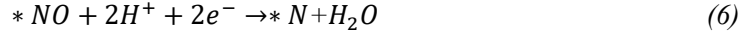
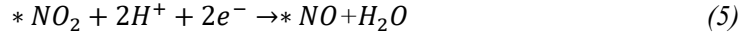
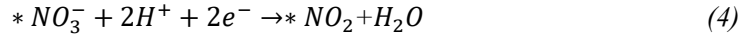
$$\text{FE}_{NH_3} = (8F \times c_{NH_4^+} \times V) / (M_{NH_4^+} \times Q) \quad (2)$$

Where  $c_{NH_4^+}$  is the concentration of  $NH_4^+$  calculated via UV-vis, in mg  $L^{-1}$ ; V is the volume of the electrolyte, t is the reaction time, in h; m is the load mass of the sample on the working electrode, mg; F is Faraday's constant, 96485 C  $mol^{-1}$ ; Q is the total charge passing through the working electrode.

## 2. Calculation details

The DFT calculations were carried out utilizing the Perdew-Burke-Ernzerhof (PBE) generalized gradient approximation (GGA) function within the CASTEP code of Materials Studio 2020 (Accelrys Software Inc., U.S.A.), and the plane-wave expansion was employed with a kinetic energy cutoff set to 500 eV, a k-point mesh of  $3 \times 3 \times 1$  was used.<sup>3-5</sup> The  $CeO_2$  surface model was constructed using a  $2 \times 2$  supercell, with a vacuum layer thickness set to 15 $\text{\AA}$ .<sup>6</sup> The total energy, force and displacement convergence was set to  $1 \times 10^{-5}$  eV/atom, 0.03 eV  $\text{\AA}^{-1}$ , and 0.001  $\text{\AA}^{-1}$  respectively.<sup>7</sup> And the chemical

reaction considered can be summarized with the reaction equations below.<sup>8-10</sup>



Where \* represents the active site, and the change in free energy of the reaction can be obtained from the following equation:

$$E_{ad} = E_t - E_s - E_m \quad (11)$$

$$\Delta G = E_{ad} + \Delta E_{ZPE} - T\Delta S \quad (12)$$

where  $E_{ad}$  is the adsorption energy,  $E_t$  is the total energy of the adsorbate-slab system, and  $E_s$  is the energy of the clean slab, and  $E_m$  is the energy of the isolated adsorbate.  $\Delta E_{ZPE}$  and  $T\Delta S$  represent zero-point energy and entropy, respectively. The zero-point energy and entropy of the free molecule and adsorbate are calculated using vibrational frequencies.

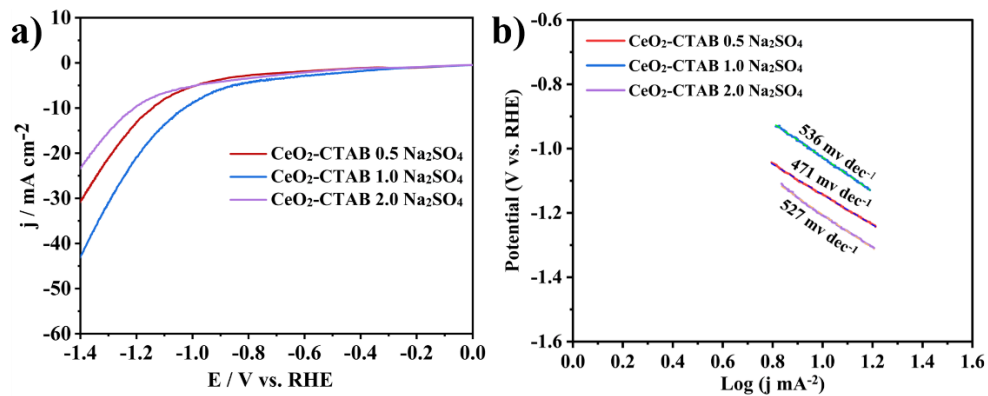


Figure S1. (a) LSV curves of three catalysts in a 0.5 M Na<sub>2</sub>SO<sub>4</sub> electrolyte, and (b) the corresponding Tafel slope.

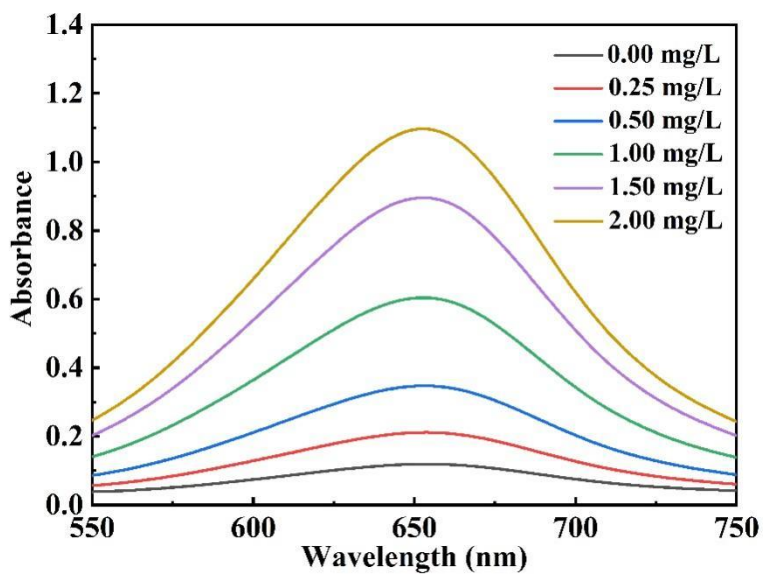


Figure S2. UV-Vis absorption spectra of various NH<sub>4</sub><sup>+</sup> concentrations.

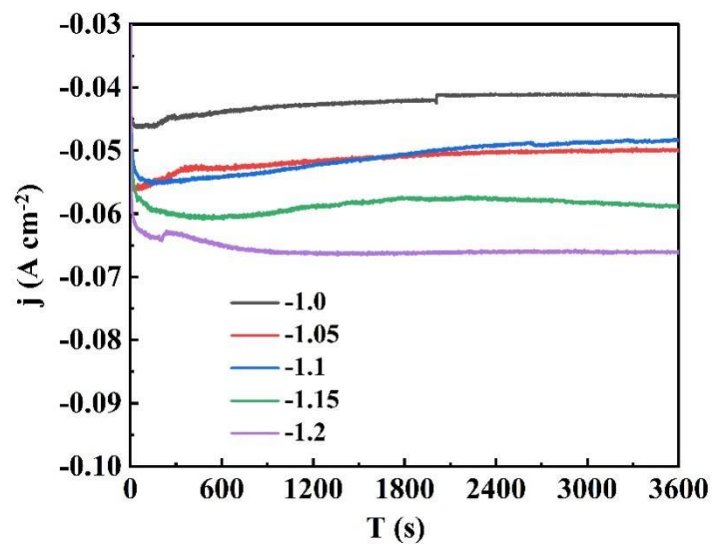


Figure S3. Chronoamperometry curves of CeO<sub>2</sub>-CTAB0.5 in a 0.5 M Na<sub>2</sub>SO<sub>4</sub> electrolyte with 0.01 M NO<sub>3</sub><sup>-</sup>.

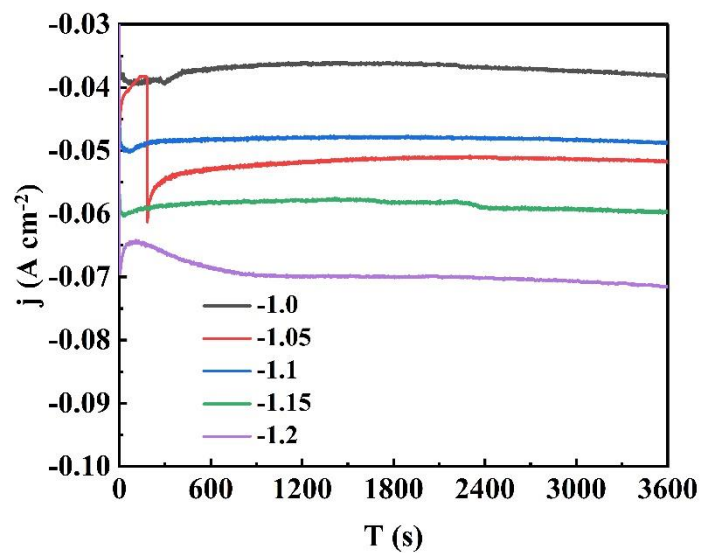


Figure S4. Chronoamperometry curves of CeO<sub>2</sub>-CTAB1.0 in a 0.5 M Na<sub>2</sub>SO<sub>4</sub> electrolyte with 0.01 M NO<sub>3</sub><sup>-</sup>.

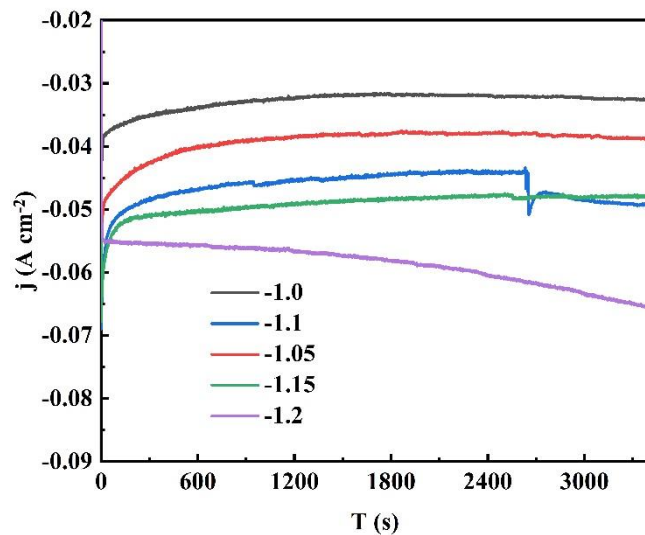


Figure S5. Chronoamperometry curves of CeO<sub>2</sub>-CTAB1.0 in a 0.5 M Na<sub>2</sub>SO<sub>4</sub> electrolyte with 0.01 M NO<sub>3</sub><sup>-</sup>.

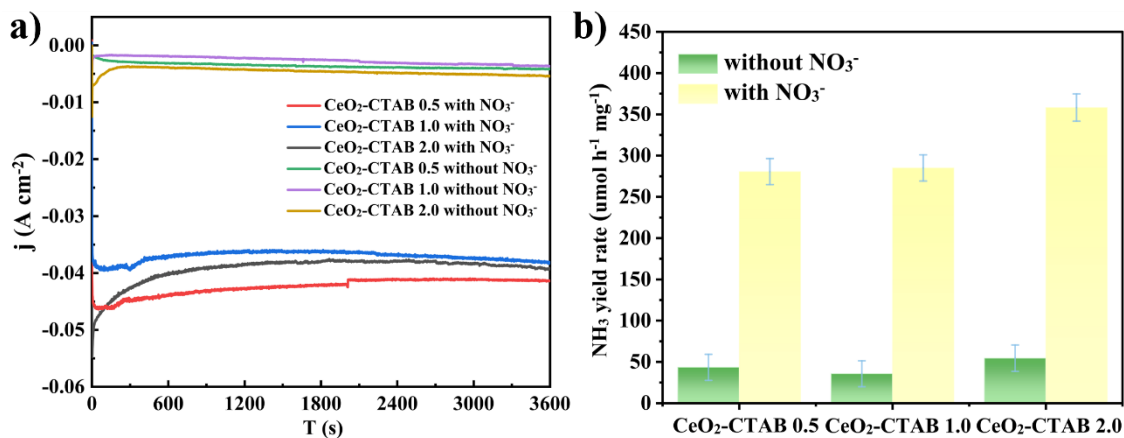


Figure S6. (a) Chronoamperometry curves and (b) Yield<sub>NH<sub>3</sub></sub> of various catalysts in electrolytes with and without NO<sub>3</sub><sup>-</sup>.

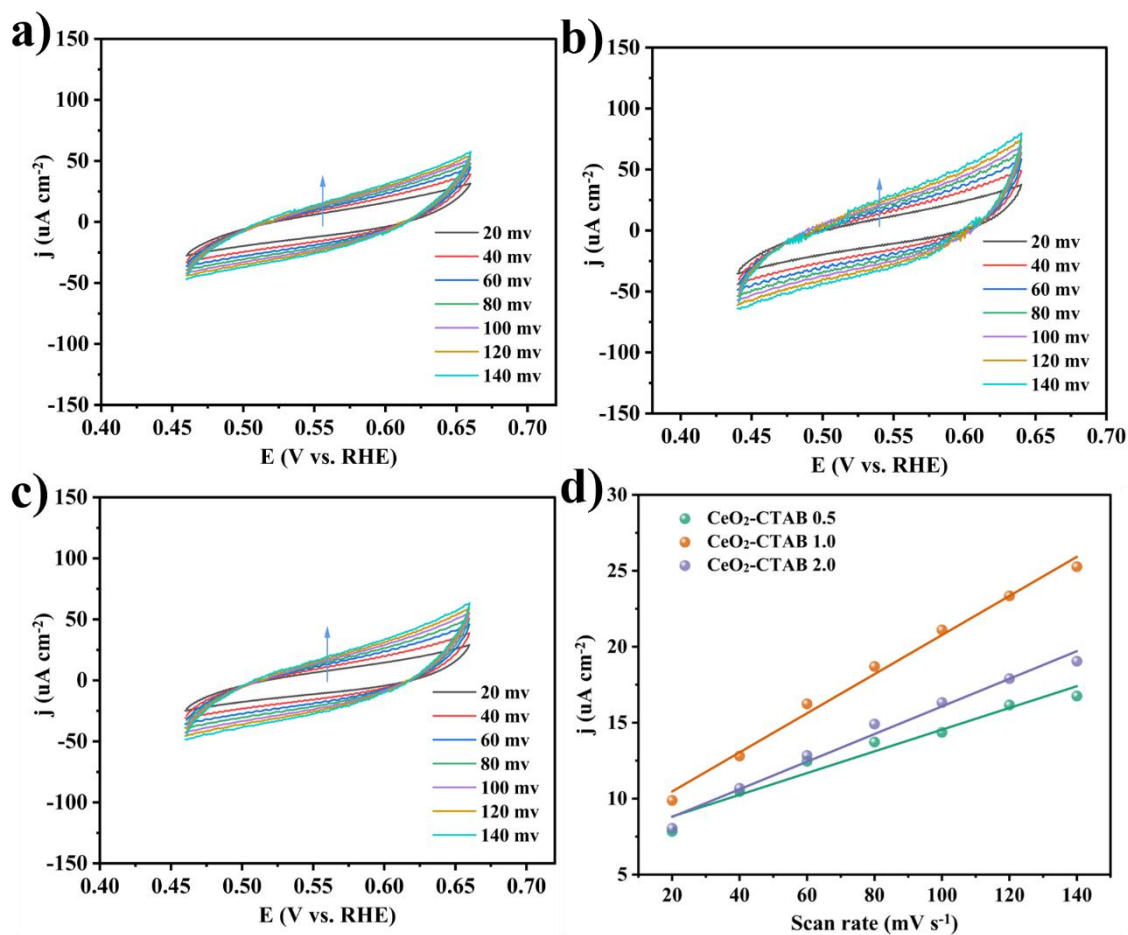


Figure S7. CV curves of (a) CeO<sub>2</sub>-CTAB0.5, (b) CeO<sub>2</sub>-CTAB1.0 and (c) CeO<sub>2</sub>-CTAB2.0 at various scanning rate, and (d) corresponding fitting curves.

Note: The specific capacitance of CeO<sub>2</sub>-CTAB0.5, CeO<sub>2</sub>-CTAB1.0 and CeO<sub>2</sub>-CTAB2.0 are fitted to be 0.07, 0.13 and 0.09 mF cm<sup>-2</sup> respectively. The specific capacitance for a flat surface is generally found to be in the range of 20-60 μF cm<sup>-2</sup>. In the following calculations of electrochemical active surface area we assume 40 μF cm<sup>-2</sup>. Therefore, we calculated the electrochemical active area (ECSA) of each catalyst as follows:

$$A_{ECSA}^{CeO_2-CTAB0.5} = \frac{0.07 \text{ mF}^{-2}}{40 \text{ uF cm}^{-2} \text{ per cm}^2_{ECSA}} = 1.75 \text{ cm}^2_{ECSA}$$

$$A_{ECSA}^{CeO_2-CTAB1.0} = \frac{0.13 \text{ mF}^{-2}}{40 \text{ uF cm}^{-2} \text{ per cm}^2_{ECSA}} = 3.25 \text{ cm}^2_{ECSA}$$

$$A_{ECSA}^{CeO_2-CTAB2.0} = \frac{0.09 \text{ mF}^{-2}}{40 \text{ uF cm}^{-2} \text{ per cm}^2_{ECSA}} = 2.25 \text{ cm}^2_{ECSA}$$

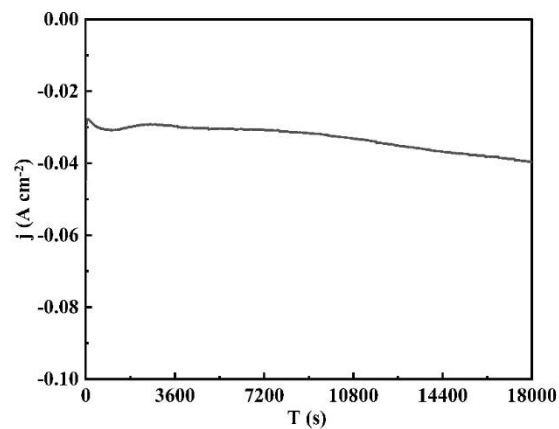


Figure S8. Long-term stability test of CeO<sub>2</sub>-CTAB2.0.

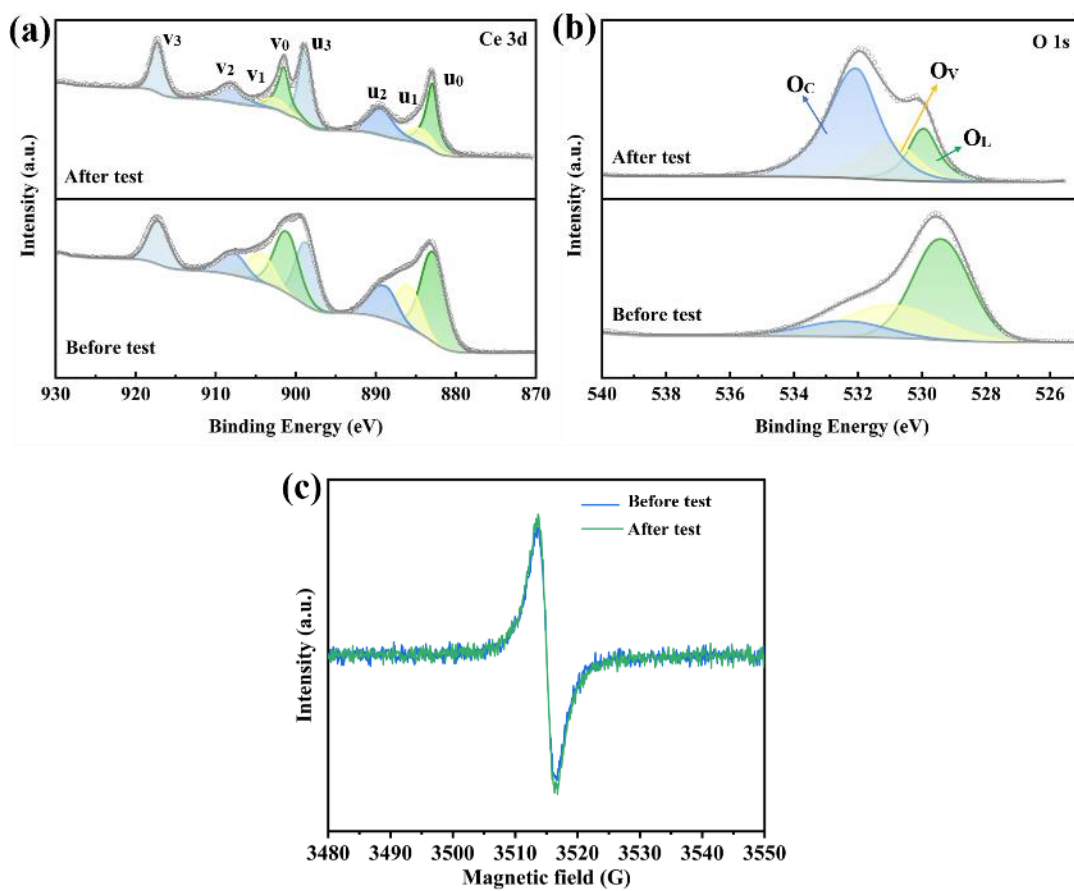


Figure S9. (a) XPS Ce 3d, (b) O 1s and (c) EPR spectra of CeO<sub>2</sub>-CTAB2.0 at before and after testing.



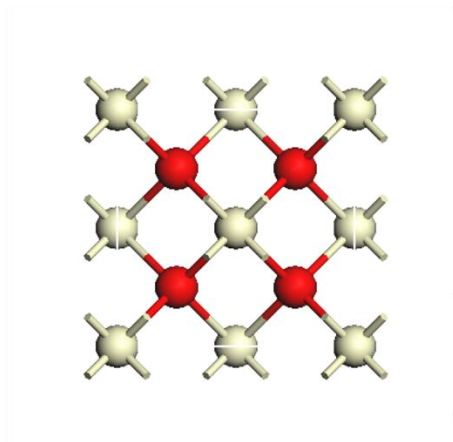


Figure S10. Atomic structure of CeO<sub>2</sub>.

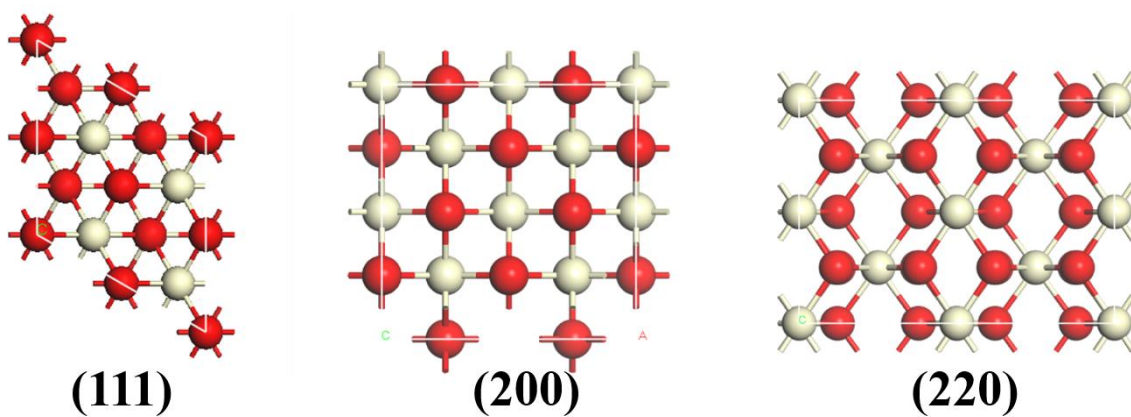


Figure S11. Atomic structure of CeO<sub>2</sub> (111), CeO<sub>2</sub> (200) and CeO<sub>2</sub> (220) slab models.

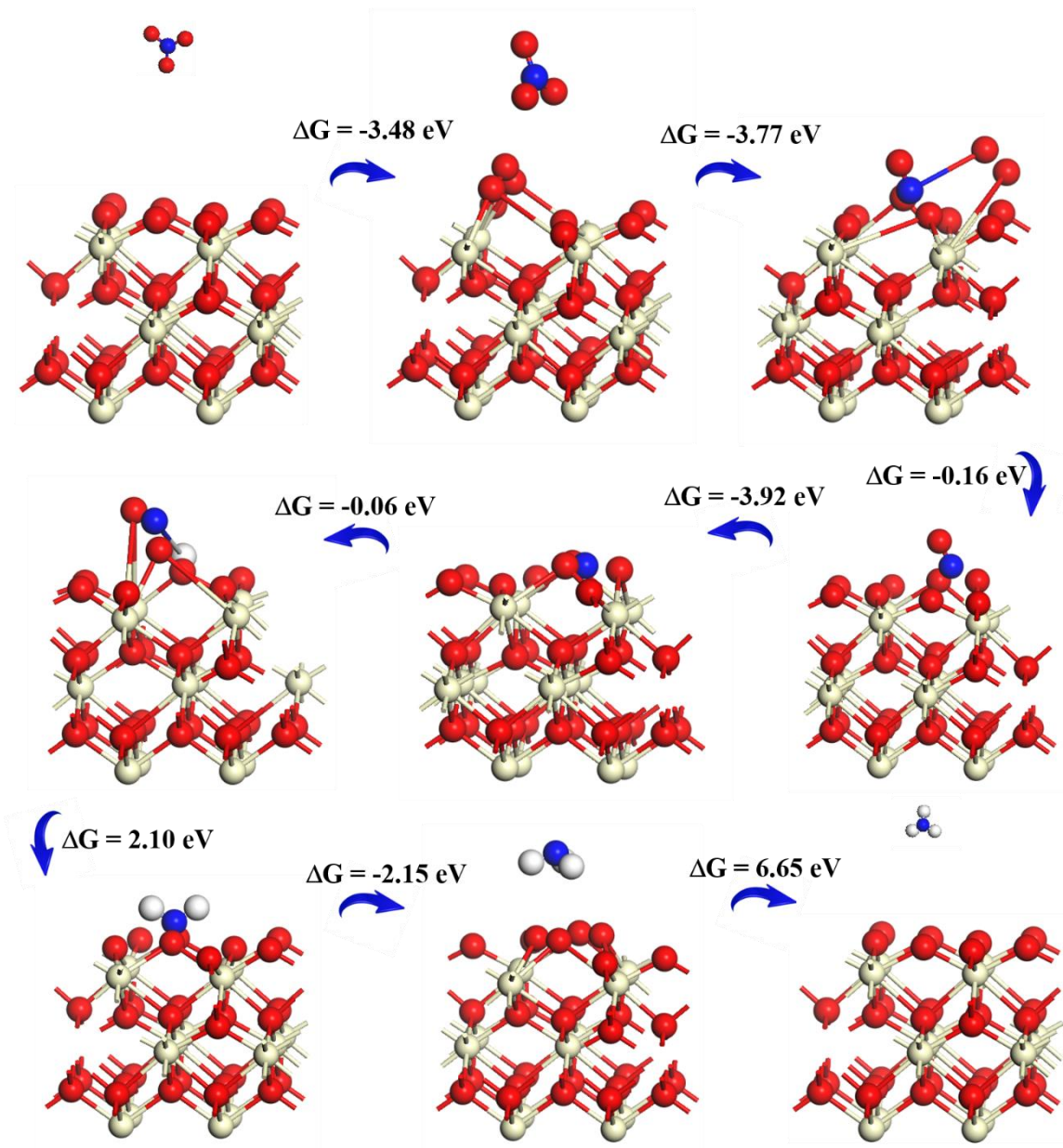


Figure S12. The optimized configurations of intermediates and corresponding free energy change involved in  $\text{NO}_3^-$  reduction on  $\text{CeO}_2$  (200) surface.

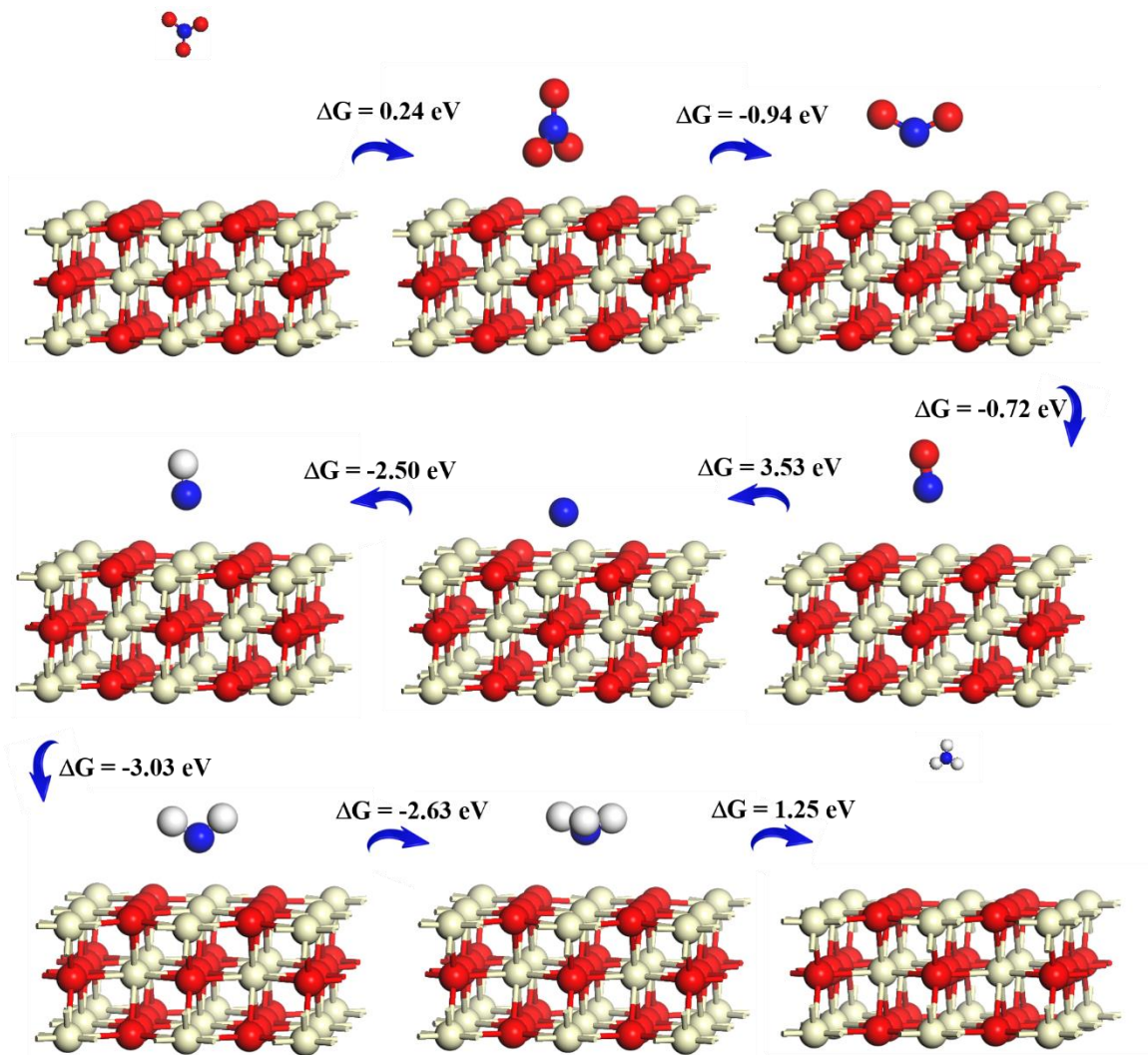


Figure S13. The optimized configurations of intermediates and corresponding free energy change involved in  $\text{NO}_3^-$  reduction on  $\text{CeO}_2$  (220) surface.

## References

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