Energy Materials

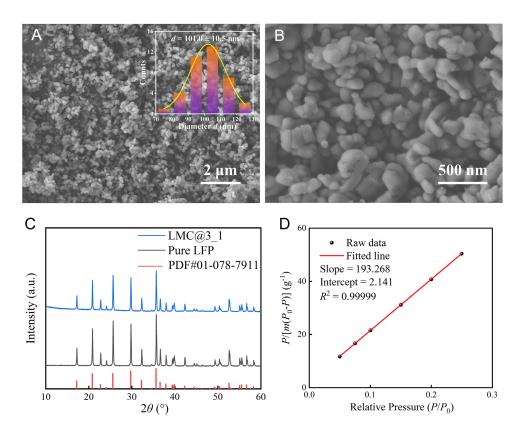
Supplementary Material

Enhancement of Li intercalation kinetics of LiFePO₄ nanoparticles with mesoporous carbon

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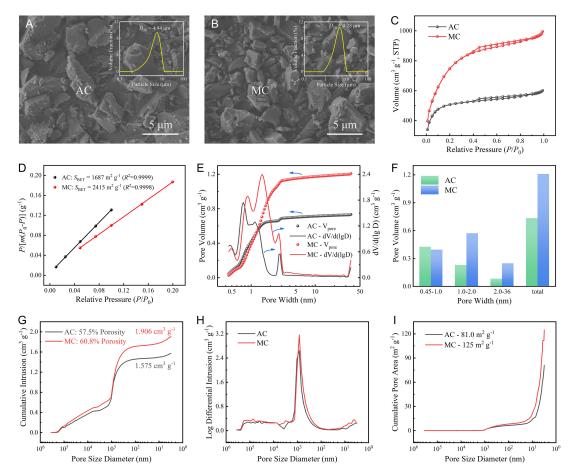
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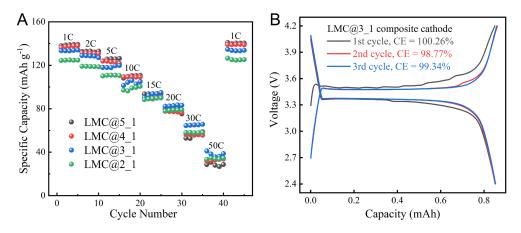
Supplementary Figure 1. Morphology, phase and pore structure characterization of LFP powders. (A–B) SEM images and particle size distribution of nano-sized LFP powders. (C) XRD pattern and the comparison to LMC@3_1 powders and standard XRD pattern (PDF No. 01-078-7911). (D) Multi-point BET linear fitting result.

The LFP spherical particles used in this work exhibited a uniform size distribution with a mean diameter of around 100 nm and a crystal structure with single phase and *Pnma* space group by comparing the standard XRD pattern. LMC@3_1 powders showed a similar XRD pattern with pure LFP powders on account of the amorphous structure of MC. The specific surface area of LFP was 10.955 m² g⁻¹ according to multipoint BET linear fitting result.



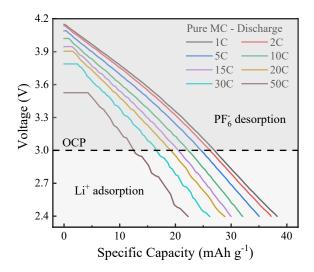
Supplementary Figure 2. Microstructure and pore structure characterization of AC and MC materials. (A–B) SEM image and particle size distribution of: (A) AC powders; (B) MC powders. (C–F) Results of the gas isothermal physical adsorption test for AC and MC powders: (C) Argon sorption isotherms at 87 K; (D) Calculation of specific surface area using BET method; (E) Pore volume and pore size distribution (QSDFT method); (F) Segmented pore volume distribution. (G–I) Results of the mercury intrusion method for AC and MC powders: (G) Cumulative intrusion volume and the porosity; (H) Pore size distribution according to differential intrusion (Log); (I) Cumulative pore area and the total specific surface area within the certain pore range.

MC maintained a similar particle size distribution and porous structure with microporous activated carbon (AC) according to the SEM images. Argon was used as adsorbate instead of nitrogen in this work to avoid the undesired effect between the pore wall and nitrogen molecule resulting from its quadrupole moment. Both AC and MC exhibited a typical type IV isotherm and a H4 type hysteresis loop at middle P/P_0 region, indicating a capillary condensation during the adsorption/desorption of liquid argon. The BET specific surface area of AC and MC were 1687 and 2415 m² g⁻¹. Using QSDFT method, the total pore volume and mesoporous ratio of MC were 1.209 cm³ g⁻¹ and 20.4%, which of AC were only 0.734 cm³ g⁻¹ and 11.0%. Mercury intrusion method was further performed to compare the pore distribution larger than 50 nm. It could be seen that the pore content of MC in the range of 2–500 nm was much more abundant than AC, which is conducive to the more electrolyte storage. Owing to sufficient supply of electrolyte and fast transfer path of ions in the large pores, the mesoporous and macro-porous structure of MC would contribute to the capacity retention, stable coulombic efficiency, and stable cycle life.

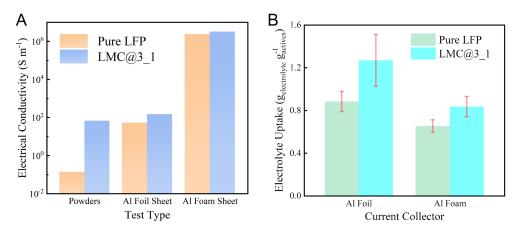


Supplementary Figure 3. (A) Rate performance of LMC cathodes with different mass ratio of MC. (B) Charge-discharge curve and coulomb efficiency (CE) of the first three cycles at 0.2C for LMC@3_1 composite cathode.

Owing to the relatively lower specific capacity of capacitive materials (MC) than battery materials (LFP), a suitable mass ratio of LFP to MC should be carefully researched to achieve the optimal electrochemical performance with both higher capacity and stronger synergistic effect, especially under high discharge rate. Rate performance test of LMC cathodes with different content of MC showed that LMC@3_1 exhibited the highest specific capacity at high discharge rate of 20C–50C, indicating that the most suitable mass ratio of LFP to MC was 3:1 to achieve the best high-power characteristic. In addition, the initial coulomb efficiency (ICE) of LMC@3_1 may be higher than 100% as observed in our test results, indicating the capacity contribution arising from the adsorption of Li-ions in MC in the later stage of the first discharge.

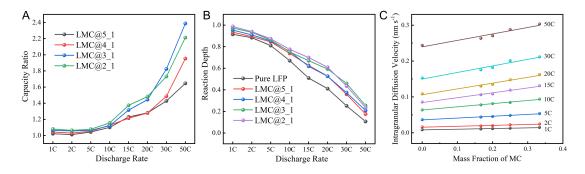


Supplementary Figure 4. Voltage-capacity curves of pure MC cathode at various discharge rates from 1C to 50C.

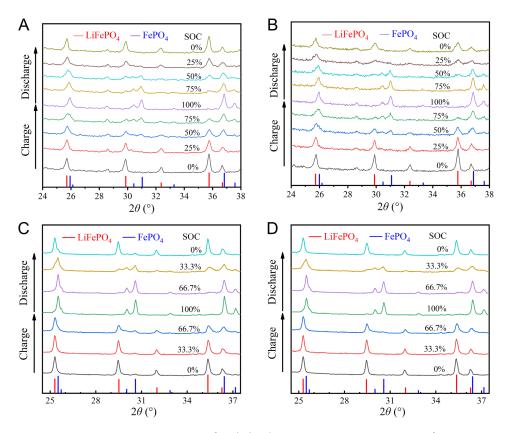


Supplementary Figure 5. (A) Comparison of electrical conductivity between pure LFP and LMC@3_1 cathodes with different test types. (B) Comparison of electrolyte uptake between pure LFP and LMC@3_1 cathodes.

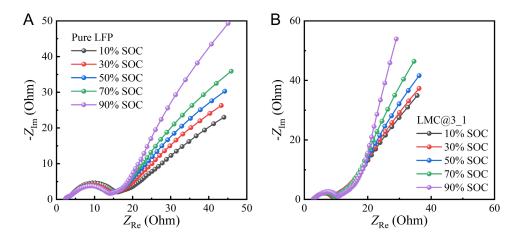
Electrical conductivity was always improved with the addition of MC no matter what test type it was. Moreover, the application of Al foam as current collector had a great increase in electrical conductivity compared to Al foil, proving that Al foam was more conducive to accelerate electron transfer and thus reduce the contact resistance between active materials and current collector. Electrolyte uptake was also improved with the addition of MC. These results indicated that MC could act as auxiliary conductive agent and electrolyte pool to accelerate the transfer of electrons and ions besides providing the capacitive effect.



Supplementary Figure 6. Analysis of the synergistic effect between LFP and MC and the Li intercalation kinetics of single LFP particle. (A) Capacity ratio of LMC composite cathodes with different mass ratio of MC under various discharge rates (for pure LFP cathode, CR = 1). (B) Reaction depth of LFP particle in pure LFP and LMC composite cathodes with different mass ratio of MC under various discharge rates. (C) Linear relationship between intragranular diffusion velocity and the mass fraction of MC in LMC composite cathodes under various discharge rates.

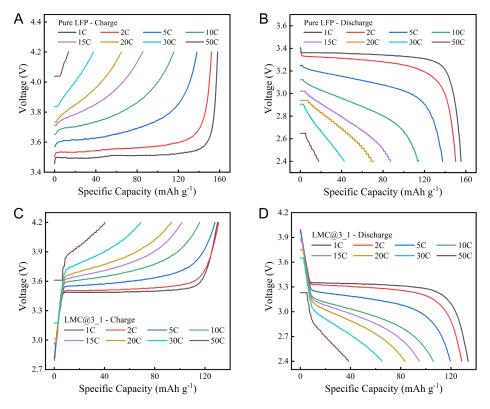


Supplementary Figure 7. A part of original *in-situ* XRD patterns of pure LFP and LMC@3_1 cathodes under two charge/discharge rates. (A) Pure LFP at 0.5C charge/discharge, (B) LMC@3_1 at 0.5C charge/discharge, (C) Pure LFP at 2C charge/discharge, (D) LMC@3_1 at 2C charge/discharge.



Supplementary Figure 8. Original EIS results at various SOC from 10% to 90%. (A) Pure LFP cathode. (B) LMC@3_1 cathode.

The EIS curves could be divided into four parts and fitted by the equivalent circuit model in Figure 5A in the main text. R_S referred to the ohmic resistance resulting from the resistance of electrolyte, electrodes, and terminals, *etc.* $C_{SEI}//R_{SEI}$ were corresponding to the solid electrolyte interface (SEI) on the LFP or Li metal surface (arc in high-frequency region), while $Q_{neg}//R_{neg}$ were related to the charge transfer process on Li metal/electrolyte interface in the anode (arc in mid-low-frequency region)^[1]. More importantly, $Q_{dI}//R_{et}$ referred to the charge transfer process on the interface of LFP/electrolyte (arc in mid-high-frequency region) and R_{et} was the charge transfer resistance, representing the difficulty for occurring electrochemical reaction. The linear part in low-frequency region was related to the Li-ion diffusive behavior inside LFP particles and expressed by a constant phase element Q_w in series.



Supplementary Figure 9. Voltage-capacity curves at various rates from 1C to 50C. (A) Pure LFP during charging test. (B) Pure LFP during discharging test. (C) LMC@3_1 during charging test. (D) LMC@3_1 during discharging test.

Current density A g ⁻¹	Specific capacity of MC mAh g ⁻¹	Specific capacitance of MC (>3.0 V) F g ⁻¹	Voltage at inflexion point V	Maximum Li ⁺ -rich concentration mol L ⁻¹	Minimum Li ⁺ -rich concentration mol L ⁻¹
0.17	38.17	84.55	3.352	0.139	0.051
0.34	37.24	83.22	3.337	0.134	0.048
0.85	35.05	79.69	3.267	0.119	0.037
1.70	32.08	75.62	3.201	0.104	0.026
2.55	30.04	72.43	3.162	0.095	0.020
3.40	28.67	70.28	3.128	0.088	0.015
5.10	26.16	64.50	3.064	0.074	0.007
8.50	22.00	55.63	2.910	0.049	0.000

Supplementary Table 1. Li⁺-rich concentration range by MC addition in

LMC@3_1 cathode

Supplementary Table 2. Ce and Ce,LFP of LMC composite cathodes with different

mass ratio	of MC	under va	rious d	ischarge rates

D - 4 -	Rate CLFP CMC	C	LMC@5_1		_1	LMC@4_1		LMC@3_1		LMC@2_1				
Kate		CLFP CMC	Ce	C _{e,LFP}	ССмс	Ce	C _{e,LFP}	<i>СС</i> мс	Ce	C _{e,LFP}	<i>СС</i> мс	Ce	C _{e,LFP}	ССмс
1C	155.50	38.17	138.75	158.87	4.58%	137.37	162.17	5.56%	133.56	165.36	7.14%	124.63	167.86	7.66%
2C	150.15	37.24	132.73	151.83	4.68%	131.14	154.62	5.68%	128.34	158.71	7.25%	118.87	159.69	7.83%
5C	137.78	35.05	125.55	143.65	4.65%	123.09	145.10	5.70%	118.63	146.49	7.39%	110.62	148.41	7.92%
10C	114.01	32.08	109.88	125.44	4.87%	109.24	128.53	5.87%	103.88	127.81	7.72%	98.55	131.79	8.14%
15C	86.59	30.04	93.75	106.49	5.34%	90.09	105.10	6.67%	92.92	113.88	8.08%	89.28	118.90	8.41%
20C	69.86	28.67	79.33	89.46	6.02%	77.17	89.30	7.43%	82.81	100.86	8.66%	78.61	103.58	9.12%
30C	42.73	26.16	55.19	61.00	7.90%	56.04	63.51	9.34%	65.00	77.95	10.06%	58.02	73.95	11.27%
50C	18.12	22.00	28.52	29.82	12.86%	32.71	35.39	13.45%	37.95	43.27	14.49%	34.07	40.11	16.14%

Notes:

(1) The unit of all capacity was mAh g^{-1} .

(2) CC_{MC} meant the capacity contribution of MC (i.e., the anion contribution or the capacitive contribution) in composite cathodes. We assumed the amounts of anions that MC could adsorb/desorb were nearly the same in pure MC cathode and LMC composite cathode, so the CC_{MC} could be calculated by:

$$CC_{\rm MC} = (C_{\rm MC} \times f_{\rm MC})/C_{\rm e} \times 100\%$$

It could be seen that CC_{MC} increased with the increase of discharge rate and the mass ratio of MC in LMC composite cathode, indicating the better rate performance of MC than LFP.

	(u) Fulle Liff cutilitute									
SOC	Rs Ω	Qd1-Y0 F s ⁿ⁻¹	$Q_{ m dl}$ -n	$R_{ m ct}$	Q_{w} -Y ₀ F s ^{$n-1$}	Q _w -n				
10%	2.437	3.5250×10^{-4}	0.8107	11.55	0.10210	0.4593				
20%	2.432	3.7568×10 ⁻⁴	0.8021	10.93	0.10444	0.4805				
30%	2.427	3.9416×10 ⁻⁴	0.7952	10.54	0.10668	0.5018				
40%	2.422	4.0986×10 ⁻⁴	0.7886	10.30	0.10792	0.5243				
50%	2.421	4.2648×10 ⁻⁴	0.7821	10.24	0.10827	0.5392				
60%	2.421	4.4326×10 ⁻⁴	0.7751	10.26	0.10835	0.5572				
70%	2.422	4.6426×10 ⁻⁴	0.7668	10.45	0.10974	0.5847				
80%	2.424	4.8100×10 ⁻⁴	0.7605	10.57	0.11249	0.6206				
90%	2.423	5.0916×10 ⁻⁴	0.7509	10.89	0.12150	0.6909				

Supplementary Table 3. The key fitting parameters of EIS results at various SOC

(a) Pure LFP cathode

(b) LMC@3_1 cathode

			<u> </u>			
SOC	Rs Ω	<i>Q</i> dl- <i>Y</i> 0 F s ^{<i>n</i>-1}	$Q_{\rm dl}$ -n	R _{ct} Ω	<i>Q</i> _{<i>w</i>} − <i>Y</i> ₀ F s ^{<i>n</i>−1}	Q _w -n
10%	2.925	3.6097×10^{-4}	0.8123	5.475	0.13808	0.6304
20%	2.936	3.6868×10 ⁻⁴	0.8082	5.483	0.13756	0.6344
30%	2.955	3.6967×10^{-4}	0.8055	5.638	0.13921	0.6508
40%	2.974	3.7184×10^{-4}	0.8017	5.890	0.14260	0.6727
50%	2.988	3.7787×10^{-4}	0.7967	6.076	0.14574	0.6928
60%	2.979	3.7134×10 ⁻⁴	0.7978	6.017	0.15065	0.7149
70%	2.993	3.7041×10^{-4}	0.7956	6.190	0.15721	0.7453
80%	3.043	3.6481×10 ⁻⁴	0.7947	6.607	0.16967	0.7910
90%	3.083	3.4100×10^{-4}	0.8018	6.869	0.19621	0.8619

Active material composition Cathode // Anode			Energy density & Power density	Cycle performance	Ref.
75%LFP+5%AC // Li	2.5–4.2	$142@0.17A\ g^{-1}\sim 70@3.4A\ g^{-1}\ ^{P}$	/	400@100%@1.7A g ^{-1 P}	[1]
12%LFP+73%AC // LTO	1.0–2.6	30@0.25C~14@10C	/	100@91%@4C	[2]
34%LFP+51%AC // LTO	1.0-2.6	37@2C ~ 20@10C	/	100@84%@4C	[3]
30%LMO+45%AC // LTO	1.2–2.8	/	16.47Wh kg ⁻¹ @4C	5000@92%@4C	[4]
65%LFP+20%AC // Li	2.8–4.2	$126.2@0.1C \sim 99.4@5C^{P}$	/	500@100%@5C	[5]
65%LFP+20%AC // Li	2.8-4.2	$110@0.172A\ g^{-1}\sim 20@17.2A\ g^{-1\ P}$	/	$500@98\%@8.6A g^{-1 P}$	[6]
60%LFP+30%CNT // Li	2.8–4.2	$110@0.011A\ g^{-1}\sim 40@2.27A\ g^{-1\ P}$	/	/	[7]
75%NCM+25%AC // Graphite	2.5–4.0	$83.5@0.034A~g^{-1}\sim 35.2@4.2A~g^{-1}~^{P}$	294Wh kg ⁻¹ @100W kg ⁻¹ 50Wh kg ⁻¹ @23kW kg ^{-1 P}	1000@95%@0.084A g ^{-1 P}	[8]
25%NCM+75%AC // HC $^{\rm L}$	2.0–4.0	$55@0.025A~g^{-1}\sim 27@5.0A~g^{-1~P}$	$75.6 \text{Wh kg}^{-1}@41.7 \text{W kg}^{-1}$ 28.5 Wh kg $^{-1}$ @6.9 kW kg $^{-1}$	$20000@98\%@0.5A g^{-1 P}$	[9]
67%NCM+33%AC // SC ^L	2.5–4.0	92.9@1C ~ 60.9@50C ^p	173.3Wh kg ⁻¹ @26.91W kg ⁻¹ 92.4Wh kg ⁻¹ @7.73kW kg ⁻¹	10000@80%@10C	[10]
80%LFP+20%AC // LTO	1.0–2.6	$96.8@0.1A\ g^{-1}\sim 57.2@5.0A\ g^{-1}\ ^{p}$	/	$500@93\%@1.0A g^{-1 P}$	[11]
28%LMO+72%AC // 19%LTO+81%AC	0.5–3.0	49@0.2C ^P	53Wh kg ⁻¹ @100W kg ⁻¹ 7.3Wh kg ⁻¹ @27kW kg ⁻¹	/	[12]
$\frac{50\% LFP + 50\% AC}{K_{1.1} Zn_{0.17} Mn_{0.83} F_{3.03}} L$	0.01–4.3	$113@0.1A\ g^{-1}\sim 68@3.2A\ g^{-1}\ ^{p}$	$81.2 \mathrm{Wh} \ \mathrm{kg}^{-1} @0.7 \mathrm{kW} \ \mathrm{kg}^{-1}$ $9.9 \mathrm{Wh} \ \mathrm{kg}^{-1} @17 \mathrm{kW} \ \mathrm{kg}^{-1}$	1000@92%@2A/g ^p	[13]
75%LFP+25%AC // KC00.54Mn0.46F3/rGO ^L	0-4.4	$125@0.1A\ g^{-1}\sim73@3.2A\ g^{-1}\ ^{p}$	229.1Wh kg ⁻¹ $@$ 0.4kW kg ⁻¹ 78.7Wh kg ⁻¹ $@$ 12.2kW kg ⁻¹	1000@89%@1A/g ^P	[14]
20%LFP+80%AC // HC $^{\rm L}$	2.2–3.8	$58.4@0.5C \sim 30@60C^{P}$	$30Wh kg^{-1}@5W kg^{-1}$ 5.7Wh kg^{-1}@2kW kg^{-1} F	30000@90%@60C	[15]
25%NCM+75%AC // HC $^{\rm L}$	2.2-3.8	$62.4@0.7C \sim 26.8@36C$ ^P	$20 Wh \ kg^{-1} @ 0.7 C \ ^{F}$	20000@90%@18C&36C	[16]
20%LFP+80%AC // HC $^{\rm L}$	2.2-3.8	$65@7mA~g^{-1} \sim 12@7.2A~g^{-1~P}$	/	100000@92%@60C	[17]
20%LFP+80%AC // HC $^{\rm L}$	2.2–3.8	/	$21 Wh kg^{-1}@10W kg^{-1}$ $2.8 Wh kg^{-1}@5 kW kg^{-1}$ F	15000@99%@5A	[18]
40%NCM+60%AC // HC $^{\rm L}$	2.2–3.8	/	$30Wh kg^{-1}@10W kg^{-1}$ $3.0Wh kg^{-1}@5kW kg^{-1}$ F	40000@92%@5A	[19]
30%LFP+70%AC // HC $^{\rm L}$	2.2–3.8	$75@0.01A\ g^{-1}\sim 30@3A\ g^{-1\ P}$	90Wh kg ⁻¹ $@$ 30W kg ⁻¹ 30Wh kg ⁻¹ $@$ 3kW kg ⁻¹	$62000@80\%@1.0A g^{-1 P}$	[20]
80%LMO+5%AC // 80%LTO+5%AC	1.5–2.7	56.4@0.5C ~ 40.7@5C	$60 Wh kg^{-1} @5 W kg^{-1} \\ 30 Wh kg^{-1} @2.5 kW kg^{-1} F$	2000@77.5%@5C	[21]
67%LFP+33%PB-AC850 // Li	2.7–4.2	130@0.2C ~ 88.2@10C ^p	200Wh kg ⁻¹ @100W kg ⁻¹ 90Wh kg ⁻¹ @10kW kg ⁻¹ ^P	500@93.4%@5C	[22]
77%NCM+3%CA // Li	2.5-4.2	$163.8@0.036A~g^{-1} \sim 126.8@1.8A~g^{-1}~^{P}$	/	$300@72.79\%@0.18A g^{-1}$	[23]

Supplementary Table 4. The electrochemical performance of reported hybrid Li-ion battery-capacitors

80%NCM+5%AC // Graphite	2.8-4.25	$150@0.018~A/g \sim 71.8@1.44~A/g$ $^{\rm P}$	/	100@78.46%@0.18 A/g ^P	[24]
20%LFP+80%AC // LTO	1.0–2.5	$75@0.02A/g \sim 45@8A/g$ ^P	90 Wh kg ⁻¹ @15W/kg 45 Wh kg ⁻¹ @15kW/kg	2000@75%@1A/g ^P	[25]
75%LFP+25%MC // Li	2.4-4.2	133.6@0.17A g^{-1} 82.8@3.4A g^{-1} 38.0@8.5A g^{-1} P	$\begin{array}{l} 437.4 Wh \ kg^{-1} @ 568.5 W \ kg^{-1} \\ 239.2 Wh \ kg^{-1} @ 9.8 kW \ kg^{-1} \\ 104.5 Wh \ kg^{-1} @ 23.4 kW \ kg^{-1} \end{array}$	$1000@100\%@1.7A g^{-1 P}$	This work

Notes: (1) Superscript "L" meant the anode had been processed with pre-lithiation before electrochemical test. (2) Superscript "P" meant

the data was calculated based on the total mass of active materials in the cathode, Superscript "F" meant the data was calculated based on

the total mass of full-cell device and other data was calculated based on the total mass of active materials both in the cathode and anode.

(3) "*n*C" meant the discharge process was completed within 1/n hour.

Supplementary Calculation 1. Li⁺-rich concentration by MC addition

Assuming the specific capacitance of MC adsorbing/desorbing PF_6^- was the same in pure MC cathode and LMC@3_1 cathode, we can derive the Li⁺-rich concentration by MC addition in LMC@3_1 cathode according to the specific capacity of MC in pure MC cathode at various current densities as follows.

For pure MC cathode, the OCP was around 3.0 V vs. Li/Li⁺ and the whole voltage range was 2.4–4.2 V, so the adsorption/desorption of PF_6^- and Li⁺ occurred in 3.0–4.2 V and 2.4–3.0 V, respectively (Supplementary Figure 4)^[26]. Considering the higher capacitance of PF_6^- adsorption/desorption in porous carbon than that of Li^{+[27]}, we calculated the specific capacitance of MC according to the voltage-capacity curve higher than 3.0 V (corresponding to the adsorption/desorption of PF_6^-). Taking discharge at 1C (equaled to 0.17 A g⁻¹) as an example, the initial voltage was 4.150 V and the specific capacity was 27.01 mAh g⁻¹ when the voltage decreased to 3.0 V, so the specific capacitance of MC at 1C could be determined as:

$$27.01 \div (4.150 - 3.0) \times 3.6 = 84.55 \text{ F g}^{-1}$$

According to the charge conservation, we considered that there were $x \mod PF_6^$ anions adsorbed at the pore surface of MC if $x \mod$ electrons passing through the circuit in pure MC cathode, thus generating $x \mod$ free Li-ions in the electrolyte.

For LMC@3_1, the discharge curve in Figure 1C in the main text showed the voltage at inflexion point was 3.352 V. Since the adsorption and desorption of PF_6^- in LMC@3_1 could occur both in the whole range higher than OCP and in some range lower than OCP, we could firstly obtain the maximum Li⁺-rich mole number (based on the mass of MC) at the inflexion point when considering the adsorption/desorption of PF_6^- occurring in the entire voltage range:

 $84.55 \times (3.352 - 2.4) \div 96485 = 8.342 \times 10^{-4} \text{ mol g}^{-1}$

For LMC@3_1 electrode, the load density of active materials (LFP and MC) and the mass fraction of MC were 0.371 g cm⁻³ and 25%, and the porosity of electrode was 55.8% according to the mercury intrusion method. Assuming that the pores in the

electrode was filled with electrolyte, then the Li⁺-rich concentration in LMC@3_1 electrode could be determined as:

$$8.342 \times 10^{-4} \times 0.371 \times 25\% \div 55.8\% \times 10^{3} = 0.139 \text{ mol } \text{L}^{-1}$$

If considering the adsorption/desorption of PF_6^- only occurring in the range of 3.0–4.2 V, then the minimum Li⁺-rich concentration in LMC@3_1 electrode could be determined as:

$$84.55 \times (3.352 - 3.0) \div 96485 \times 0.371 \times 25\% \div 55.8\% \times 10^3 = 0.051 \text{ mol } \text{L}^{-1}$$

The actual Li⁺-rich concentration in LMC@3_1 electrode should be somewhere between the above maximum and minimum values. The Li⁺-rich concentration and relevant data at other current densities were listed in Supplementary Table 1. The specific capacitance of MC and the voltage at inflexion point were acquired from Supplementary Figure 4 and Supplementary Figure 9D.

Supplementary Calculation 2. Li-ion diffusion coefficient according to EIS tests

The linear part in low-frequency region of EIS result is related to the Li-ion diffusion behavior and the corresponding solid-phase Li-ion diffusion coefficient (D_{Li^+} , cm² s⁻¹) could be calculated by the following equation^[28]:

$$D_{\text{Li}^{+}} = \frac{R^2 T^2}{2n^4 F^4 A^2 C_0^2 \sigma_w^2}$$
 Equation (S1)

Here, *R* is the gas constant (8.314 J mol⁻¹ K⁻¹), *T* is the absolute temperature (K), *n* is the electron transfer number (n = 1 for LFP), *F* is the Faraday constant (96485 C mol⁻¹), *A* is the active area involved in electrochemical reaction and calculated by multiplying the specific surface area of LFP and its mass in the cathode (cm²), *C*₀ is the Li-ion molar concentration in the active material ($C_0 = 7.69 \times 10^{-3}$ mol cm⁻³ for LFP)^[28], σ_w is the Warburg factor (Ω s^{-0.5}), which equals to the slope of the linear fitting of *Z*_{Re} to $\omega^{-0.5}$ in low-frequency region (0.01–0.1 Hz in this work), as shown in the inset of Figure 5A in the main text.

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