

## Supporting Information

**Scissor g-C<sub>3</sub>N<sub>4</sub> for high-density loading of catalyst domains in mesoporous thin-layer conductive network for durable Li-S batteries**

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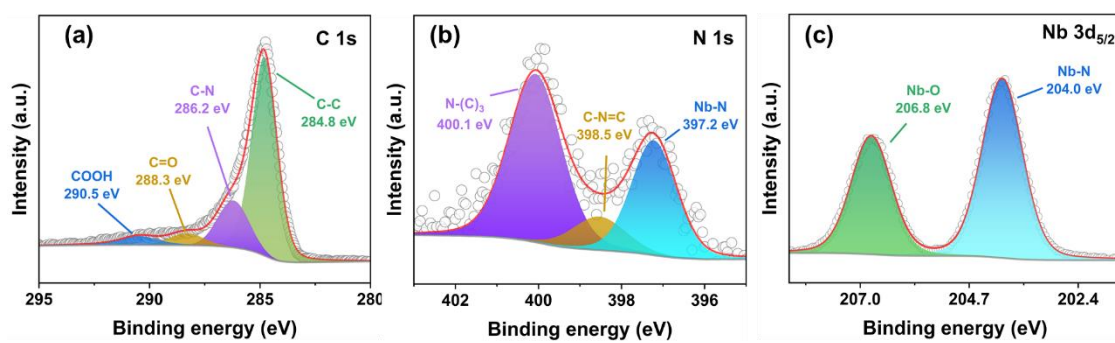
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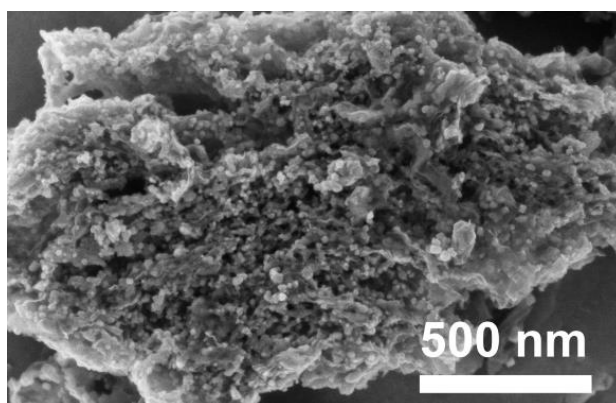
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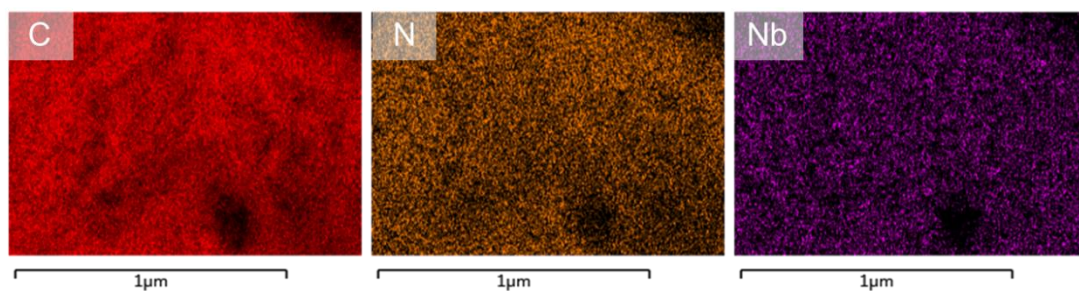
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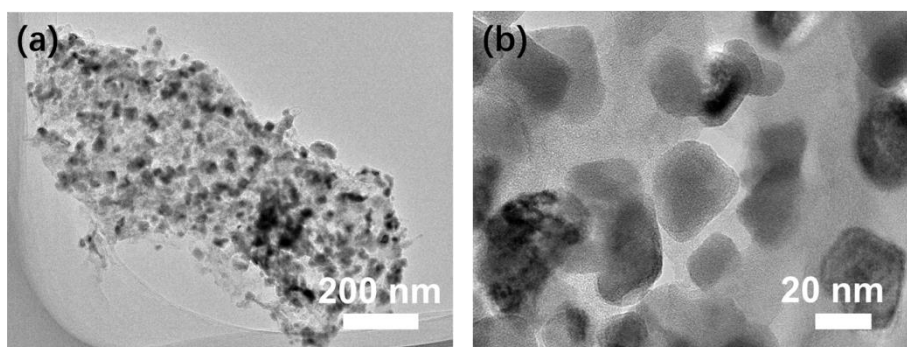
**Figure S1.** XPS results of as-synthesized NbN/C powder: (a) C 1s, (b) N 1s, (c) Nb 3d<sub>5/2</sub>.



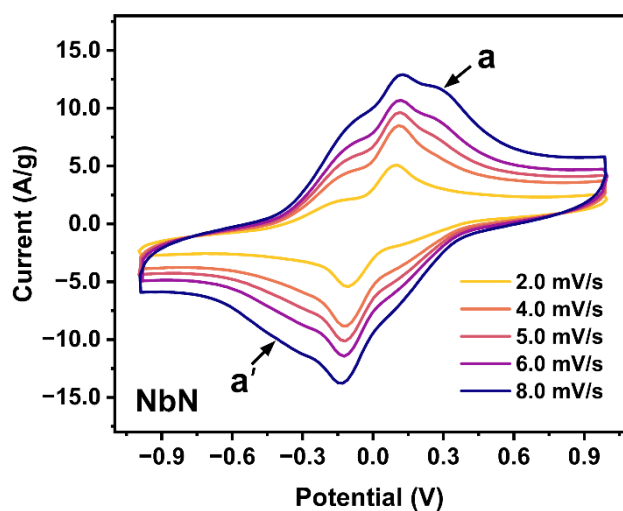
**Figure S2.** SEM image of as-synthesized NbN/C powder.



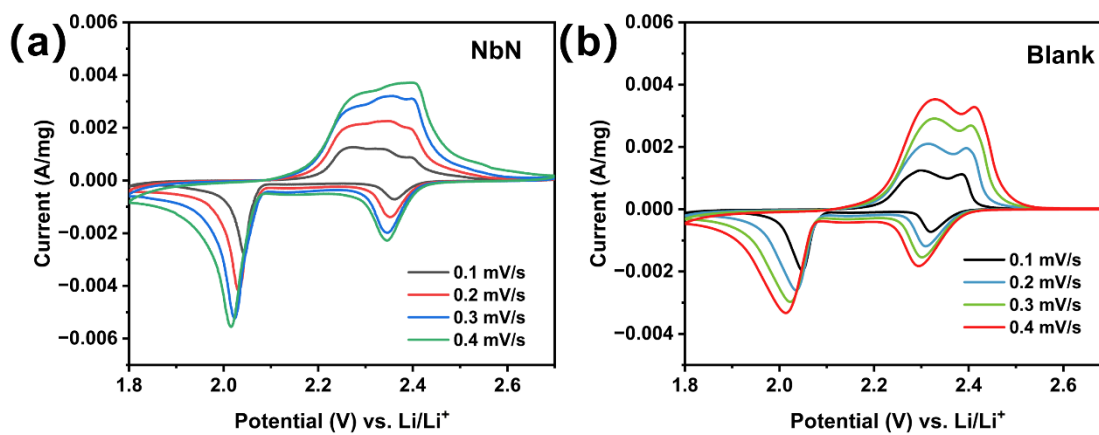
**Figure S3.** EDS mapping of as-synthesized NbN/C powder.



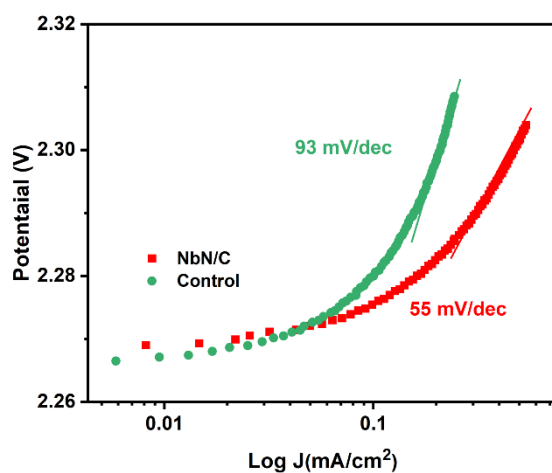
**Figure S4.** TEM images of as-synthesized NbN/C powder in different scales.



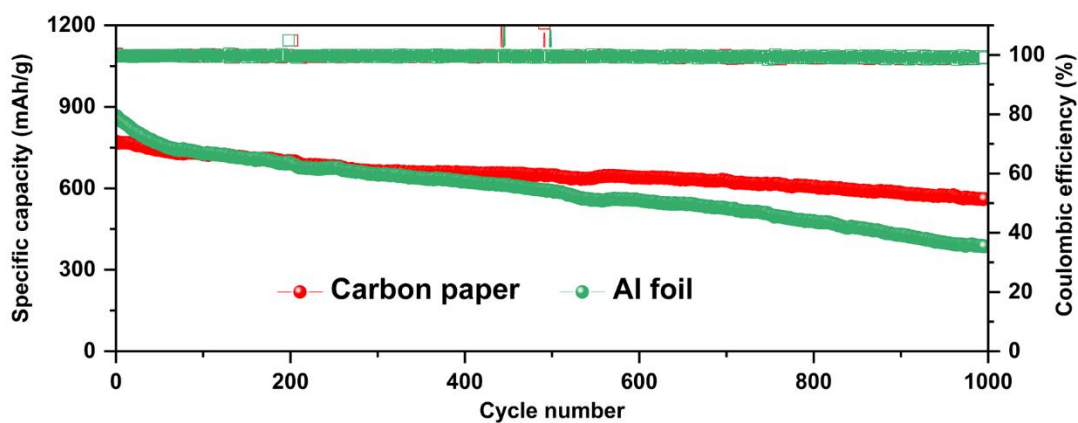
**Figure S5.** CV test on the symmetric Li|Li cell with the NbN/C@PP separator at different scan rates from 2.0 to 8.0  $\text{mV s}^{-1}$ .



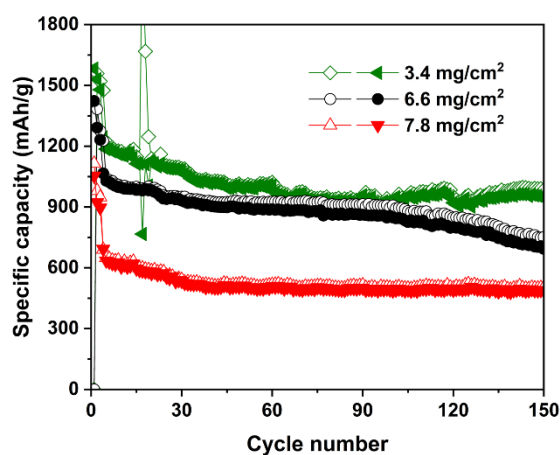
**Figure S6.** CV tests on the Li-S cells based on different separators of (a) NbN/C@PP and (b) pristine PP at different scan rates from 0.1 to 0.4 mV s<sup>-1</sup>.



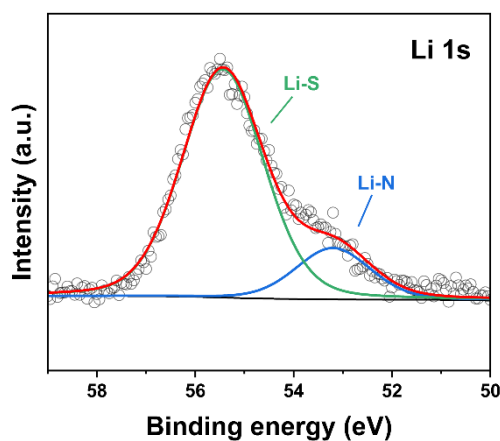
**Figure S7.** Tafel plots of the Li-S cells based on different separators corresponding to the oxidation stage from Li<sub>2</sub>S<sub>n</sub> to sulfur.



**Figure S8.** Electrochemical performance of Li-S cells with different current collectors under a rate of 2 C.



**Figure S9.** Electrochemical performance of Li-S cells with different high S-mass loading cathodes.



**Figure S10.** XPS result of Li 1s for the cycled NbN/C@PP separator.

**Table S1.** Comparison of adsorption energies of LiPSs on the surfaces of different materials.

Materials	Adsorption energy (eV)						Reference
	Li <sub>2</sub> S	Li <sub>2</sub> S <sub>2</sub>	Li <sub>2</sub> S <sub>4</sub>	Li <sub>2</sub> S <sub>6</sub>	Li <sub>2</sub> S <sub>8</sub>	S <sub>8</sub>	
NbC (001)	—	—	—	-2.91	—	—	Ref. S1
NiO (111)	—	—	-2.39	-2.36	-3.14	—	Ref. S2
NbN (111)	—	—	-5.21	-2.74	-4.63	—	Ref. S3
NbN (200)	—	—	-3.54	—	—	—	Ref. S4
VN (200)	-3.86	-3.14	-3.27	-3.01	-3.46	-2.21	Ref. S5
<b>NbN (200)</b>	<b>-3.07</b>	<b>-3.04</b>	<b>-2.09</b>	<b>-2.53</b>	<b>-3.12</b>	<b>-2.04</b>	<b>This work</b>

**Table S2.** Energy barriers at different stages of conversion reactions based on various LiPSs obtained from the calculated Gibbs free energies.

Conversion step	$S_8 \rightarrow Li_2S_8$	$Li_2S_8 \rightarrow Li_2S_6$	$Li_2S_6 \rightarrow Li_2S_4$	$Li_2S_4 \rightarrow Li_2S_2$	$Li_2S_2 \rightarrow Li_2S$
Energy barrier (eV)	-3.42	0.53	0.7	0.39	0.81

**Table S3.** Mass fractions of cell components and E/S ratio, N/P capacity ratio.

Battery container	Mass fraction of battery component				E/S ratio ( $\mu\text{L}/\text{mg}$ )	N/P capacity ratio
	NbN/C@PP	Lithium anode	S cathode	Electrolyte		
2.53 g	0.00635 g	0.0188 g	0.00522 g	0.034 g	—	—
97.3%	0.244%	0.723%	0.201%	1.31%	5	8.31

**Table S4.** The performance comparison of high loading sulfur batteries.

S loading ( $\text{mg}/\text{cm}^2$ )	E/S ratio ( $\mu\text{L}/\text{mg}$ )	Current density (1 C = 1672 mA/g)	Cycle number	Capacity retention (mAh/g)	Reference
7.6	5.0	0.05 C	40	605.3	Ref. S6
4.06	5.0	1 C	500	340.4	Ref. S7
5.6	10	0.1 C	30	732.1	Ref. S8
5.3	9.43	0.1 C	45	754.7	Ref. S9
5.8	4.0	0.1 C	55	730	Ref. S10
5.4		0.2 C	80	703.7	Ref. S11
5.8	5.2	0.2 C	100	775.9	Ref. S12
6.6	7.0	0.2 C	100	686.2	Ref. S13
6.6	5.0	1 mA/cm <sup>2</sup> (~0.1 C)	100	850	This work

**Note S1.** Detailed information on how to get the activation energy difference for modified and control cells based on the Tafel plots.

According to the CV tests in Figure 4a under a scan rate of 0.2 mV s<sup>-1</sup>, the relationship between electrode potential and activation energy for the NbN/C modified or blank PP based cell can be calculated according to the equation:

$$E_a = E_a^0 + \alpha ZF \varphi_{cathode}(O_X/Red)_{IR} \quad (1)$$

where  $E_a$  is the activation energy of reduction process,  $E_a^0$  is the intrinsic activation energy,  $\alpha$  is the symmetry coefficient,  $Z$  is the number of charge transfer,  $F$  is the

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Faraday's constant, and  $\varphi_{cathode}(O_X/Red)_{IR}$  is the irreversible potential during cycling.

According to the simplified Tafel equation:

$$\eta_{cathode} = a + b \ln j_{cathode} \quad (2)$$

where  $\eta_{cathode}$  is the overpotential of cathode and  $j_{cathode}$  is the current density of cathode, a and b are the factors that are determined according to the specific system.

Here  $b = -\frac{RT}{\alpha ZF}$  is obtained from the slope of Tafel curve in Figure 4d, 4e and S5.

Putting  $b$  into the Equation (1), a new equation can be obtained as follows:

$$E_a = E_a^0 - \frac{RT}{b} \varphi_{cathode}(O_X/Red)_{IR} \quad (3)$$

Hence, the difference on the activation energies of the reductions from  $S_8$  to  $Li_2S_n$  (denoted as  $E_{a1}$  and  $E_{a1}'$ ) and from  $Li_2S_n$  to  $Li_2S$  (denoted as  $E_{a2}$  and  $E_{a2}'$ ) for the modified and control cells are:

$$\Delta E_{a1} = E_{a1} - E_{a1}' = -8.63 \text{ kJ mol}^{-1}$$

$$\Delta E_{a2} = E_{a2} - E_{a2}' = -19.08 \text{ kJ mol}^{-1}$$

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